# **POLK STATE COLLEGE**

WINTER HAVEN, FLORIDA



# CHILLER PLANT EVALUATION

April 2, 2014

C&A# 5747

CARASTRO & ASSOCIATES, INC.

2609 W. DE LEON STREET, TAMPA, FLORIDA 33609

WWW.CARASTRO.COM

# **TABLE OF CONTENTS**

SECTI	IONS PAGE
I.	SCOPE OF WORK2
II.	EXECUTIVE SUMMARY WITH RECOMMENDATIONS2
III.	EXISTING CONDITIONS - MECHANICAL2
IV.	EXISTING CONDITIONS - ELECTRICAL
V.	CHILLER PLANT SCHEMES4
	A. SCHEME ONE DESCRIPTION5
	B. SCHEME ONE DIAGRAM6
	C. SCHEME TWO DESCRIPTION7
	D. SCHEME TWO DIAGRAM8
	E. SCHEME THREE DESCRIPTION9
	F. SCHEME THREE DIAGRAM10
	G. SCHEME FOUR DESCRIPTION11
	H. SCHEME FOUR DIAGRAM12
VI.	HEATING HOT WATER SYSTEM DESCRIPTION13
	A. HEATING SCHEME ONE15

Appendix A	LIFE CYCLE COST ANA	ALYSIS16
Appendix B	Condenser Water Trea	atment23

# I. SCOPE OF WORK

1. Carastro & Associates was commissioned to perform a review of the existing chiller plant to determine the best chiller plant replacement strategy that would yield the most value for Polk State College.

# **II. EXECUTIVE SUMMARY AND RECOMMENDATIONS**

- 1. The intent of this study is to determine the type of chiller plant that would offer most benefits on a Life Cycle basis. For this report, the size (in tonnage) of the new plant is not the primary focus, as long as the chiller plant tonnage is reasonably close to the actual size and consistent throughout all schemes.
- 2. The size of the proposed chiller plant was estimated through several avenues. First, all of the facilities served by the chiller plant were surveyed to document the HVAC equipment and electrical systems. Second, a model was developed using a DOE approved load simulation software and adjusted to match the existing conditions for the chiller plant. Lastly, the model was revised to account for full student occupancy, building occupancy schedules, future expansion, and ASHRAE compliant ventilation rates. The following steps were followed:
  - a) The current chiller plant has a total capacity of 650 tons, while the connected load of all chilled water air handlers appears to be approximately 970 tons. The latter was estimated based on actual Test & Balance data (where available), model numbers of equipment (where available) and tonnage assumptions based on chilled water coil sizes.
  - b) A preliminary calculation for code compliant ventilation rates was also performed based on the overall building areas and occupancy rates provided to us. This load was estimated to 270 tons.
  - c) It is believed that the existing building HVAC systems do not meet current codes in terms of ventilation rates. The current capacity of the plant (650 tons) and a portion of the outside air load (200 tons) were summed together to obtain the total required tonnage. An additional 350 tons was added to this total for future build outs, which brought the plant tonnage to a total of 1,200 tons. It is estimated that the extra tonnage would be sufficient for 70,000 to 95,000 square feet of new construction. A smaller chiller plant may also be considered for the initial build out and future chillers added as the campus grows.
- Based on the results of the LCCA see Data Sheet 3 in Appendix A a water-cooled plant with centrifugal chillers, cooling towers, variable primary chilled water flow and constant condenser water flow, has the **lowest first cost** and the **lowest life cycle cost over 25 years**. Based on these findings, a water-cooled plant that is efficient, scalable and requires minimal maintenance is recommended.

# **III. SUMMARY OF EXISTING CONDITIONS - MECHANICAL**

 The existing central energy plant is located in the Multi-Services building (WMS) and serves nine facilities throughout the Polk State College, Winter Haven campus. The facilities include: Administration (WAD), Fine Arts (WFA), Student Center (WST), Science & Math (WSC), Multi-Services (WMS), Rehabilitation (WRH), Criminal Justice (WCJ), Learning Resources (WLR), and Health Center (WHC).

- 2. The central energy plant consists of a chilled water system and a heating hot water system. The chiller system is a primary/secondary chilled water loop system. The boiler system is a primary heating hot water loop system.
- 3. The chiller plant consists of three water cooled centrifugal chillers, three cooling towers, three thermal storage tanks, three condenser water pumps, three primary chilled water pumps, two secondary chilled water pumps, and two chilled water storage pumps.
- 4. Chillers CH-1, CH-2 and CH-3 were installed in 1988. Chiller CH-1 is a York 150 ton chiller. Chillers CH-2 and CH-3 are both York 250 ton chillers. All three chillers still use the environmentally unfriendly R-11 refrigerant. These chillers are 26 years old, which is past the recommended service life of 23 years according to ASHRAE (American Society of Heating, Refrigerating and Air-Conditioning Engineers).
- 5. The three centrifugal chillers currently operate twenty-four hours a day, at full capacity. It has been stated during walk-throughs that the shut-down of any chiller (i.e. failure or for maintenance) results in a fairly quick increase of the campus chilled water supply temperature and insufficient cooling for the school campus. Considering the air-conditioned area of the campus is over 300,000 sq.ft., the existing chiller capacity is very low at 461 sq.ft. per ton when compared to ASHRAE's cooling load check figures for educational facilities (150 to 240 sq.ft. per ton).
- 6. Cooling towers CT-1, CT-2, and CT-3 are all Marley brand cooling towers. The capacity of cooling tower CT-1 is 150 tons, while towers CT-2 and CT-3 are 250 ton units.
- 7. The three thermal storage tanks have a capacity of 120,000 gallon storage tanks. These tanks were intended to reduce energy costs by taking advantage of off-peak electricity rates and reduce demand charges. According to personnel onsite, the control systems for these tanks were never properly completed and therefore the thermal storage system has not been utilized to its design intent potential. Their current usage is buffer tanks and, as such, they may provide a little extra chilled water capacity during a chiller failure (i.e. slow down the increase in chilled water temperature by mixing).
- 8. All existing pumps for the primary chilled water loop are constant flow pumps. The secondary chilled water loop pumps and the heating hot water pumps are equipped with variable frequency drives.
- 9. The chiller plant is controlled by an Andover Direct Digital Control (DDC) system, although the extent of the controls is limited.
- 10. The existing chilled water main supply and return piping serving the campus loop is documented as 14" diameter steel piping. Ultrasound testing results provided for our review indicated acceptable piping condition. However, a more in-depth analysis by removing a section or coupons could be performed. In terms of pipe sizing, the 14" main piping is adequate for the 1200-ton plant studied in this report.

# **IV. SUMMARY OF EXISTING CONDITIONS - ELECTRICAL**

- The existing main electrical service supplying the chiller plant and the multi services building (WMS) consists of a Polk State College owned 1000 KVA 13.2KV to 277/480V pad mounted transformer, two motor control centers and a Square D QED 2000 Amp (Main Circuit Breaker) 480V 3 Phase 4W switchboard MSB. This switchboard supplies:
  - a. Three existing chillers.

- b. Several 277/480V and 120/208V 3 Phase panel boards that supply power and lighting loads in the building. (These existing loads are not associated with the scope of this study other than by their impact on the existing electrical service).
- c. Motor Control Center MCC1 is a Square D 600 Amp 480V 3 Phase Model 5. MCC1 supplies the cooling towers and the following pumps: P-1, P-2, P-4, P-5, P-7, P-9 and HWP-1
- d. Motor Control Center MCC2 is a Square D 600 Amp 480V 3 Phase Model 5. MCC2 supplies the following pumps: P-3, P-6, P-8, P-10, and HWP-2.
- The existing Switchboard MSB is currently in violation of the National Electrical Code (N.E.C.) 240.4(C). The total ampacity of the service entrance conductors is 1530A, the main circuit breaker long time ampere rating is set for 2000A.

<u>NOTE</u>: This issue can be easily corrected for the existing conditions by adjusting the main circuit breakers long time ampere rating to (1500A). With this adjustment the existing service lateral conductors will be protected in compliance with N.E.C. It was also observed that all the other main circuit breaker's settings are set for the minimum value which may cause nuisance tripping of the main circuit breaker. This issue can be corrected by performing a selective coordination study to set the main circuit breaker properly.

- 3. Based on a calculation of existing loads the existing pad mounted 1000KVA 13.2KV to 277/480V currently serving the maintenance building is overloaded by 119.9KVA, which constitutes a violation of N.E.C. 450.3(A).
- 4. During a previous service upgrade, the existing service entrance conductors were pulled through the existing abandoned switchboard main section (converted to a pull box) and extended overhead to the now existing MSB. This constitutes a violation of N.E.C. 230.70(A)(1) which limits the length of the service entrance conductors to a point nearest the point of entrance into the building.
- 5. The existing feeders currently supplying motor control centers MCC1 and MCC2 have a total ampacity of 510A, however, these are supplied from 600A circuit breakers. While this feeder size complies with minimum N.E.C. 240.4(B) requirements it will not comply with the maximum 2% voltage drop requirements mandated by the Florida Building Code (FBC). The intent of this FBC rule is to increase the efficiency of the installation.

# V. CHILLER PLANT SCHEMES

- 1. The capacity of the new chiller plant was modeled using Carrier HAP software. The model built was developed to account for code and ASHRAE compliant ventilation rates and also allow for some future expansion of the campus. The new chiller plant for this analysis has the following characteristics:
  - 1200 tons of cooling capacity
  - o 460V/3Ph power
  - Variable primary chilled water flow
- Polk State College personnel expressed an interest in ice thermal storage. Therefore, several different schemes were developed, with and without ice storage. After a quick evaluation of their complexity and first cost, four schemes were selected for a Life Cycle Cost Analysis (LCCA). The results of this analysis are included in Appendix A; the data is summarized as follows:

- a. Page 1 includes a brief description of the systems analyzed, estimated annual costs for electricity and maintenance, as well as our opinion of probable cost for the equipment in each of the four schemes analyzed.
- b. Page 2 has a breakdown of all the equipment and their initial cost estimates, along with a calculated "present worth value" based on their replacement at a particular time within the 25-year cycle, 4% equipment cost increase at the time of replacement and 7% interest rate.
- c. Page 3 includes a summary of the Life Cycle Costs associated with the four schemes.
- d. Page 4 summarizes the HVAC costs as well as ancillary costs associated with each scheme.
- e. Page 5 includes a summary of the estimated annual electricity costs, as well as annual maintenance costs.
- f. Page 6 includes a few assumptions made while assembling the LCCA.

# SCHEME 1

# MECHANICAL

(2) 600 ton Water Cooled Centrifugal Chillers, (2) 600 ton Cooling Towers, (4) Variable flow chilled water pumps. One of the chillers is provided with a Variable Frequency Drive (i.e. for better, more efficient handling of part load conditions), and the second machine is constant speed (i.e. better efficiency at full load).

# **ELECTRICAL**

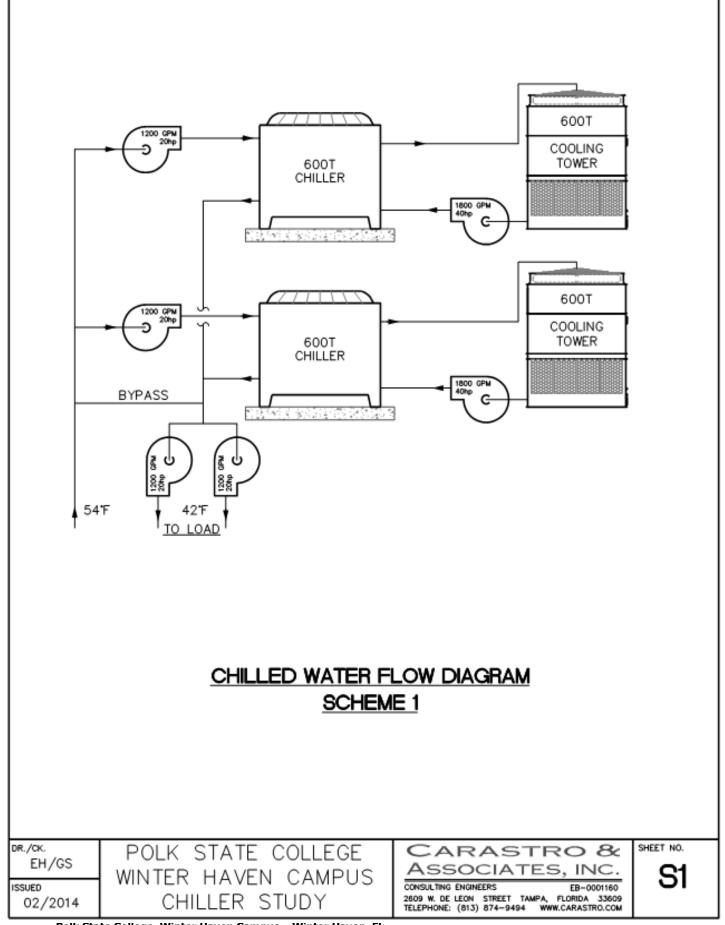
- a. The projected load of the new equipment will impose additional load on the transformer. The existing 1000KVA transformer will have to be replaced with a new 1500KVA transformer.
- b. The existing switchboard MSB (two sections) may be reused. A new 2000A main circuit breaker shall be provided to replace the existing pull box. Replace the existing service entrance conductors from a new pad mounted transformer to the new main and from the new main to the existing MSB. The ampacity of these new service entrance conductors shall be no less than 2000A in order to use the full capacity of the existing MSB. The ground electrode system and the neutral to equipment ground connection shall be established at the new main circuit breaker location as required by N.E.C. 250.50. Provide new 600A feeders for motor control centers MCC1 and MCC2. These recommendations will be sufficient to comply with N.E.C. as well as Florida Building Code.

# ADVANTAGES

- Water-cooled centrifugal chillers are significantly more efficient than air-cooled equipment.
- Proven system, relatively easy to operate and maintain
- Lowest first cost

#### DISADVANTAGES

- More equipment to maintain when compared to all air-cooled schemes (i.e. no cooling towers)
- Chemical treatment for condenser water



Polk State College, Winter Haven Campus – Winter Haven, FL Chiller Plant Evaluation

# SCHEME 2

### **MECHANICAL**

(1) 600 ton Water Cooled Centrifugal Chiller with Variable Frequency Drive, (1) 600 ton Cooling Tower, (2) 225 ton Air-Cooled Chillers, (18) Ice Storage Tanks, (1) Heat Exchanger, (7) Variable flow chilled water pumps

# **ELECTRICAL**

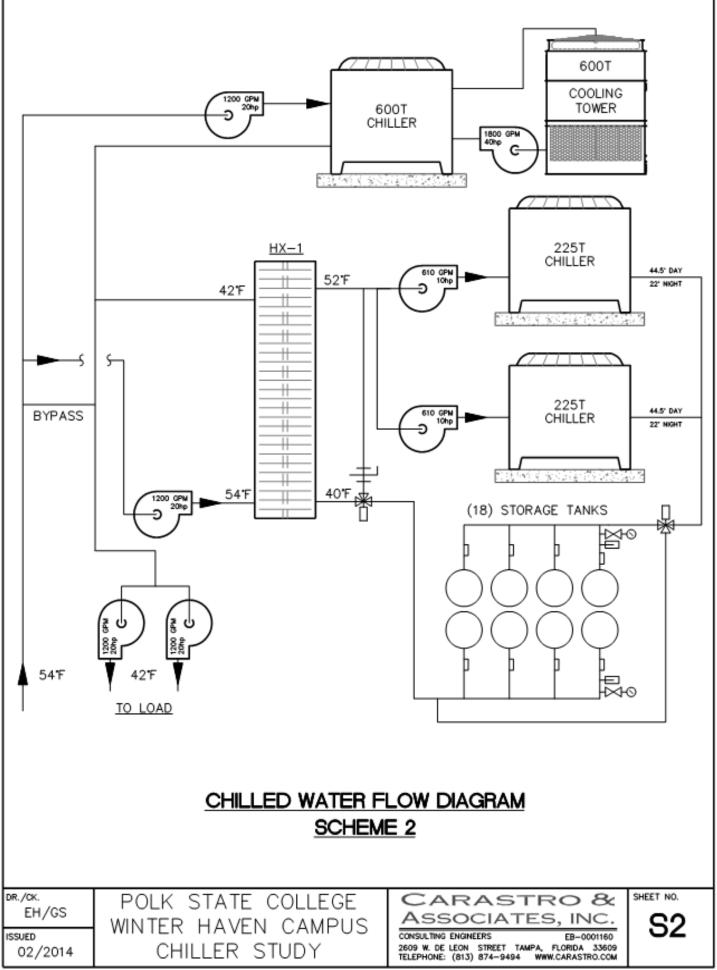
- a. The projected load of the new equipment will impose additional load on the transformer. The existing 1000KVA transformer with a new 1500KVA transformer.
- b. The existing switchboard MSB (two sections) may be reused. A new 2000A main circuit breaker shall be provided to replace the existing pull box. Replace the existing service entrance conductors from a new pad mounted transformer to the new main and from the new main to the existing MSB. The ampacity of these new service entrance conductors shall be no less than 2000A in order to use the full capacity of the existing MSB. The ground electrode system and the neutral to equipment ground connection shall be established at the new main circuit breaker location as required by N.E.C. 250.50. Provide new 600A feeders for motor control centers MCC1 and MCC2. These recommendations will be sufficient to comply with N.E.C. as well as Florida Building Code.
- c. The existing motor control centers MCC1 and MCC2 may be reused. There will be a cost associated with the electrical demolition of the existing equipment and wiring to chillers, pumps, etc. as well as new circuit breakers and starters that need to be provided to accommodate the new equipment's power requirements.

# **ADVANTAGES**

- Water cooled centrifugal chillers are significantly more efficient than air-cooled equipment.
- Rebate from power company
- Reduction in demand charges

#### DISADVANTAGES

- Complex scheme, due to mix of water-cooled and air-cooled chillers
- More equipment to maintain: chillers, pumps, heat exchanger
- Chemical treatment for condenser water
- Higher first cost



Polk State College, Winter Haven Campus – Winter Haven, FL Chiller Plant Evaluation

# SCHEME 3:

# MECHANICAL

(3) – 350 ton High Efficiency Air Cooled Screw Chillers, (30) Ice Storage Tanks, (1) Heat Exchanger, (5) Variable flow chilled water pumps

# **ELECTRICAL**

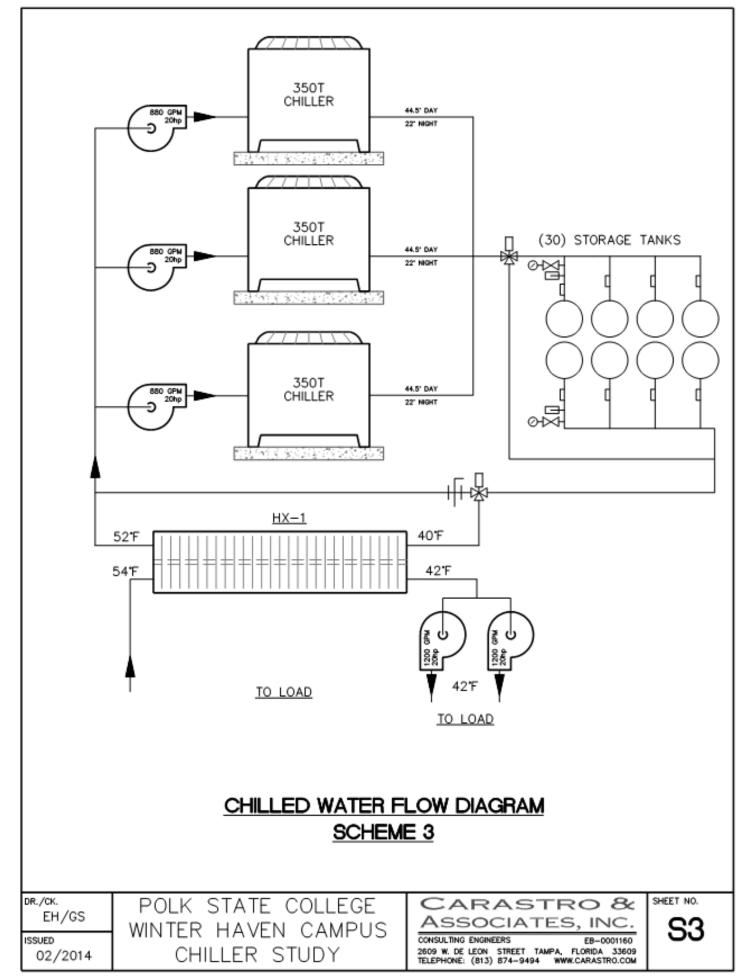
- a. The projected load of the new equipment will impose additional load on the transformer. The existing 1000KVA transformer with a new 2000KVA transformer.
- b. Based on the additional loads, the service entrance conductors and the main service switchboard will have to be upgraded. A new 2500A main circuit breaker shall be provided to replace the existing pull box. Replace the existing service entrance conductors from a new pad mounted transformer to the new main and from the new main to a new 2500A double distribution section (to be installed at the existing MSB distribution section location). The ampacity of these new service entrance conductors shall be no less than 2500A. The ground electrode system and the neutral to equipment ground connection shall be established at the new main circuit breaker location as required by N.E.C. 250.50. Provide new 600A feeders for motor control centers MCC1 and MCC2. These recommendations will be sufficient to comply with N.E.C. as well as Florida Building Code.

# **ADVANTAGES**

- Air-cooled equipment is simple to operate and maintain.
- Rebate from power company
- Reduction in demand charges
- No condenser water

#### DISADVANTAGES

- Operating ice storage requires in-depth knowledge of building's load profile in order to maximize benefits and reduce energy consumption.
- More equipment to maintain: chillers, pumps, heat exchanger
- Higher first cost



# SCHEME 4:

### MECHANICAL

(1) – 300 ton Premium Efficiency Air Cooled Screw Chiller, (2) – 350 ton High Efficiency Air Cooled Screw Chillers, (24) Ice Storage Tanks, (1) Heat Exchanger, (6) Variable flow chilled water pumps

# **ELECTRICAL**

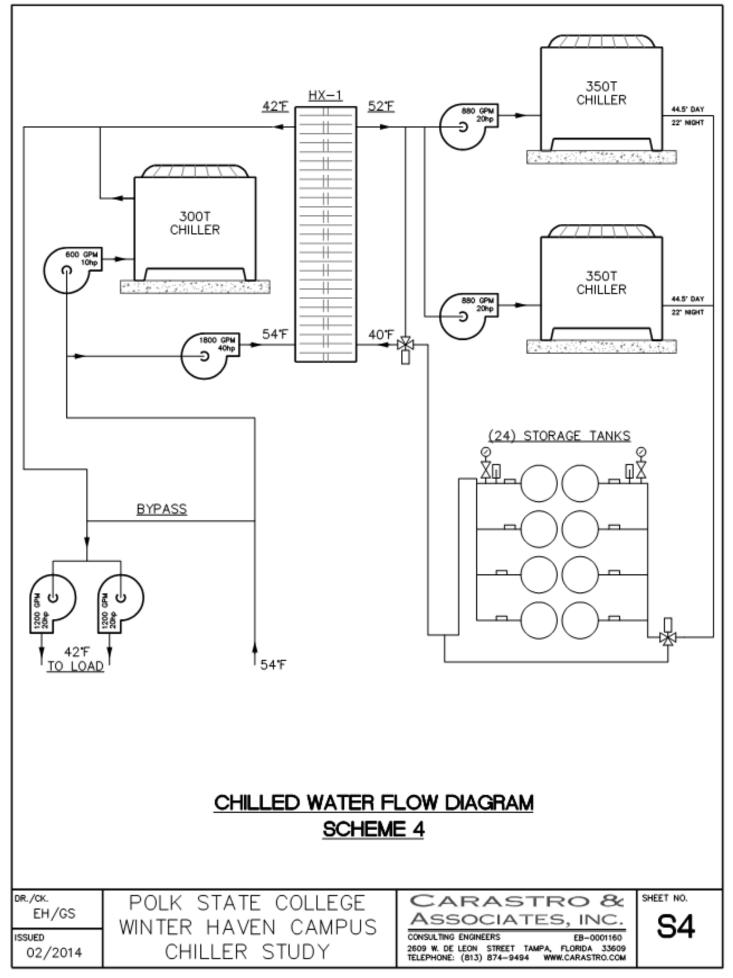
- a. The projected load of the new equipment will impose additional load on the transformer. The existing 1000KVA transformer with a new 2000KVA transformer.
- b. Based on the additional loads, the service entrance conductors and the main service switchboard will have to be upgraded. A new 2500A main circuit breaker shall be provided to replace the existing pull box. Replace the existing service entrance conductors from a new pad mounted transformer to the new main and from the new main to a new 2500A double distribution section (to be installed at the existing MSB distribution section location). The ampacity of these new service entrance conductors shall be no less than 2500A. The ground electrode system and the neutral to equipment ground connection shall be established at the new main circuit breaker location as required by N.E.C. 250.50. Provide new 600A feeders for motor control centers MCC1 and MCC2. These recommendations will be sufficient to comply with N.E.C. as well as Florida Building Code.
- c. The existing motor control centers MCC1 and MCC2 can be reused. There will be a cost associated with the electrical demolition of the existing main switchboard MSB, equipment and wiring to chillers, pumps etc. as well as new circuit breakers and starters that need to be provided to accommodate the new equipment's power requirements.

#### **ADVANTAGES**

- Air-cooled equipment is simple to operate and maintain.
- Rebate from power company
- Reduction in demand charges
- No condenser water
- More efficient air-cooled chiller on the building side

#### DISADVANTAGES

- Operating ice storage requires in-depth knowledge of building's load profile in order to maximize benefits and reduce energy consumption.
- More equipment to maintain: chillers, pumps, heat exchanger
- Higher first cost

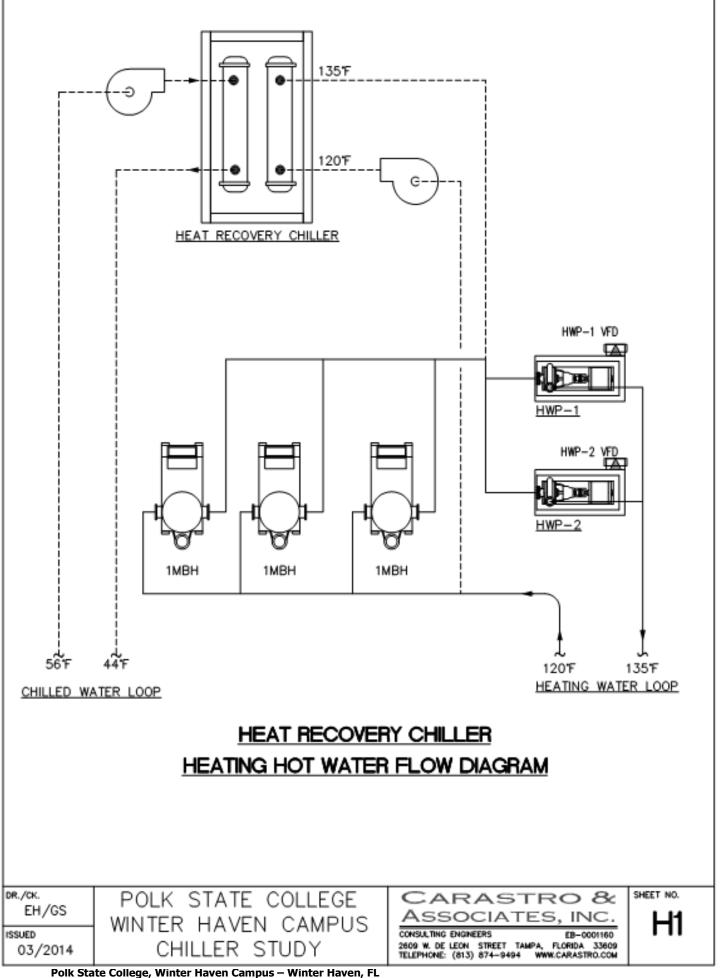


# VI. HEATING HOT WATER - HEAT RECOVERY CHILLER SYSTEM

- 1. The existing boiler system consists of three boilers and two heating hot water pumps. Boilers B-1, B-2, & B-3 were all installed in 2008. The two heating hot water pumps operate with variable frequency drives. All three boilers are Aerco 1,000,000 BTUH forced draft boilers. These boilers are high efficiency condensing boilers and are fueled by natural gas.
- Since the boilers are fairly new, replacement is not necessary. However, it would be beneficial to consider adding a Heat Recovery Chiller (HRC). The data below indicates that this upgrade would have a quick payback – i.e. two years, after which it would continue to offer an estimated twenty-four thousand dollars in operational cost savings year after year.
- 3. The primary task of this machine is to provide heating hot water. The HRC is connected to the chilled water return piping and its byproduct is cold chilled water, thus reducing the work of the main chillers. In the case of a new chiller plant, a reduction in size of the cooling chillers is also an option.
- 4. For the purpose of this study, we selected a 70-ton Multistack unit, which has a heating output similar to one of the existing boilers. The net heating capacity of the MS070 chiller is 880,300 BTUh, while the cooling capacity is 635,000 BTUh, or 53 tons. Below are our estimated costs and payback analysis for both, the existing plant and the new plant (i.e. chillers efficiencies are different:

	EX	ISTING PLANT		
Chiller Efficiency	Electricity Cost			
kw/ton	\$/kwh			
0.825	\$0.10			
Boiler Efficiency	Cost per Therm	Cost per 100 MBTUh	Cost per 880 MBTUh	
80%	\$1.10	\$1.38	\$12.10	
	HEAT RI	ECOVERY CHILLER		
Chiller	Electricity Cost	Heat BTUh	Cost to produce 880 MBTUh	
kw	\$/kwh			
72.5	\$0.10	880300	\$7.25	
Heating BTUh	Cooling BTUh	Equivalent Chiller Plant Tons		
885000	635000	53		
savings from not usin	g the main boiler and	running the HRC	\$4.85	
cost of tons of cooling	g produced by main p	lant in same hour	\$4.37	
total savings from usi	ing the HRC		\$9.22	
Hours per year	Cost savings per hour	Cost savings per year	Cost of chiller	Simpl payba
2700	\$9.22	\$24,894	\$50,000	

		NEW PLANT			
Chiller Efficiency	Electricity Cost				
kw/ton	\$/kwh				
0.6	\$0.10				
Boiler Efficiency	Cost per Therm	Cost per 100 MBTUh	Cost per 880 MBTUh		
80%	\$1.10	\$1.38	\$12.10		
	HEAT R	ECOVERY CHILLER			
Chiller	Electricity Cost	Heat BTUh	Cost to produce 880 MBTUh		
kw	\$/kwh				
72.5	\$0.10	880300	\$7.25		
Heating BTUh	Cooling BTUh	Equivalent Chiller Plant Tons			
885000	635000	53			
savings from not usir	ng the main boiler and	running the HRC	\$4.85		
	g produced by main p		\$3.18		
total savings from usi	total savings from using the HRC \$8.03				
Hours per year	Cost savings per hour	Cost savings per year	Cost of chiller	Simple paybacl	
2700	\$8.03	\$21,679	\$50,000	2.	



# **APPENDIX A**

# LIFE CYCLE COST ANALYSIS

#### CHILLER PLANT UPGRADES - POLK STATE COLLEGE C&A # 5747

#### Data Sheet 1

#### SYSTEM DESCRIPTION

Scheme 1	(2) Water Cooled Chillers, (2) Cooling Towers, variable primary flow
	(1) Water Cooled Chiller, (1) Cooling Tower, (2) Air Cooled Chillers, (18) Ice Tanks, (1) Heat Exchanger
Scheme 3	(3) Air Cooled Chillers, (30) Ice Tanks, (1) Heat Exchanger
Scheme 4	(3) Air Cooled Chillers, (22) Ice Tanks, (1) Heat Exchanger

#### ASSUMED ENERGY UNIT COSTS

Fuel Type	Units	BTU/Unit	Unit Cost
Electric	KWh	3,413	\$0.06148
Demand charge	KWh	3,413	\$10.30

#### ANNUAL OPERATING COSTS

Scheme	Maintenance	Maintenance	Operating	Electrical
	Supplies	Labor	Labor	Consumption
Scheme 1	\$5,000	\$10,000	included	\$283,454
Scheme 2	\$5,500	\$10,500	included	\$375,081
Scheme 3	\$2,000	\$6,000	included	\$436,804
Scheme 4	\$2,000	\$6,000	included	\$381,259

#### HVAC SYSTEM INSTALLED COSTS\*

(GROSS FROM DATA SHEET 4)		
Scheme 1	\$2,021,280	
Scheme 2	\$2,477,920	
Scheme 3	\$2,460,320	
Scheme 4	\$2,448,360	

Engineer:	Carastro & Associates, Inc.
Date:	March 4, 2014

The costs listed on this page represent the engineer's opinion of probable cost. A licensed contractor should be consulted for accurate construction costs. <u>REFER TO PAGE 6 FOR A LIST OF ASSUMPTIONS MADE.</u>

#### LIFE CYCLE COST ANALYSIS

#### CHILLER PLANT UPGRADES - POLK STATE COLLEGE C&A # 5747

Data Sheet 2

SINGLE EXPENDITURE DATA PWF is multiplier from Single Expenditure Chart Present Worth = (Item Cost in Today's Dollars) x CPI x AF x PF x PWF (1) (2) (3) (4) Item Name CPI PF PWF Scheme Year Item Cost AF Present Worth Chillers 23 \$660,000 2.4647 0.0887 1,8080 0.2109 \$55,018 1 0.0944 \$285,000 4.1002 \$62,456 (2) Cooling Towers 20 2.1911 0.2584 0.2584 0.0944 20 \$30,000 2.1911 \$6,574 (4) Pumps 4.1002 DDC 15 \$106,400 1.8009 0.1098 7.0236 0.3624 \$53,553 1.8080 (1) 600-ton WC Chiller 23 \$370,000 2.4647 0.0887 0.2109 \$30,844 2 \$143,000 \$31,338 2 1911 4,1002 20 0.0944 0.2584 (1) Cooling Towers (2) 225-ton AC Chillers 15 \$325.00 1.8009 0.1098 7.0236 \$163,577 0.3624 \$43,000 20 2 1911 0.0944 4,1002 0.2584 (7) Pumps \$9,423 (18) Ice Tanks 20 \$305,000 2.1911 0.0944 4.1002 0.2584 \$66,839 \$112,000 2.1911 0.0944 4,1002 \$24,544 (1) Heat Exchanger 20 0.2584 Glycol System 15 \$8,000 1.8009 0.1098 7.0236 0.3624 \$4,027 15 \$145.20 1.8009 0.1098 7.0236 0.3624 \$73,081 DDC (3) 350-ton AC Chillers \$675,000 \$339,738 3 15 1.8009 0.10 7.023 0.3624 (5) Pumps \$32,000 2.1911 0.094 4.1002 0.2584 \$7,013 20 2.1911 0.2584 (30) Ice Tanks 20 \$475,000 0.0944 4,1002 \$104,094 2.1911 4.1002 20 \$112,000 0.0944 0.2584 \$24,544 (1) Heat Exchanger 1,8009 \$4,027 15 \$8,000 0.1098 7.0236 0.3624 Glycol System 15 \$126,400 1.8009 0.10 7.023 0.3624 \$63,619 DDC (2) 350-101 + (1) 300 \$675,000 0.1098 4 ton AC Chil 15 1.8009 7.0236 0.3624 \$339,738 0.2584 (6) Pumps 20 \$40,000 2.1911 0.094 4.1002 \$8,766 0.2584 20 2.1911 \$385,000 0.0944 4.1002 \$84,371 (24) Ice Tanks 2.1911 (1) Heat Exchanger 20 \$178,000 0.0944 4.1002 0.2584 \$39,008 \$4,027 Glycol System 15 \$8,000 1.8009 0.1098 7.0236 0.3624 15 \$134,600 7.0236 0.3624 \$67,746 DDC 1,8009 0.1098

#### TOTAL MAJOR REPAIR COST

(Sum of Present Worths on this page)

Scheme 1	\$177,602
Scheme 2	\$403,673
Scheme 3	\$543,034
Scheme 4	\$543,655

Engineer:	Carastro & Associates, Inc.
Date:	March 4, 2014

Notes

(1) consumer price index; 4% cost increase at time of replacement

(2) annual payment for the life of equipment (@ 7%)

(3) lump sum of eqpm. cost for the remainder of service life from year of replacement to year 25 (@ 7%)

(4) adjustment to today's dollars (@ 7%)

The costs listed on this page represent the engineer's opinion of probable cost. A licensed contractor should be consulted for accurate construction costs. <u>REFER TO PAGE 6</u> FOR A LIST OF ASSUMPTIONS MADE.

#### LIFE CYCLE COST ANALYSIS

#### CHILLER PLANT UPGRADES - POLK STATE COLLEGE C&A # 5747

#### Data Sheet 3

#### PRESENT WORTH IN TODAY'S DOLLARS

Initial Cost = HVAC System Installed Cost Supplies = Annual Maintenance Supplies x 11.65 Labor = Annual Total Labor x 11.65 Major Repair = Total Major Repair Costs for 25 years Energy Cost = Annual Energy Cost x 12.78

#### FINANCIAL SUMMARY (Total owning and operating cost over 25-year life of school)

	Scheme 1	Scheme 2	Scheme 3	Scheme 4
Initial Cost	\$2,021,280	\$2,477,920	\$2,460,320	\$2,448,360
Supplies	\$58,250	\$64,075	\$23,300	\$23,300
Labor	\$116,500	\$122,325	\$69,900	\$69,900
Major Repair	\$177,602	\$403,673	\$543,034	\$543,655
Energy Cost	\$3,622,542	\$4,793,536	\$5,582,352	\$4,872,488
Total O&O Cost	\$5,996,174	\$7,861,529	\$8,678,906	\$7,957,703
Estimated TECO Rebate	\$0	\$86,400	\$144,000	\$115,200
Revised First Cost	\$5,996,174	\$7,775,129	\$8,534,906	\$7,842,503
Percent Increase		29.67%	42.34%	30.79%
Ranking of Schemes	1	2	4	3

Campus AC floor area Block Load Tonnage 360,000 Square Feet 1,200 Tons

Engineer: Carastro & Associates, Inc.

Date: March 4, 2014

The costs listed on this page represent the engineer's opinion of probable cost. A licensed contractor should be consulted for accurate construction costs. REFER TO PAGE & FOR A LIST OF ASSUMPTIONS MADE.

#### LIFE CYCLE COST ANALYSIS

#### CHILLER PLANT UPGRADES - POLK STATE COLLEGE C&A # 5747

#### Data Sheet 4

Net, Total	A/C Floor Ar	ea	360,000	Total A/C	Tonnage		1,200
ESTIMATED HVAC SYSTEM INSTALLED COST							
Scheme 1	\$1,439,400	Scheme 2	\$1,849,200	Scheme 3	\$1,786,400	Scheme 4	\$1,759,600
ASSOCIA	TED ESTIMA	TED CONS	TRUCTION O	OSTS			
Electrical	Service						
Scheme 1	\$417,000	Scheme 2	\$424,000	Scheme 3	\$507,000	Scheme 4	\$522,000
BUILDING	FLOOR ARE	A					
Scheme 1	\$0	Scheme 2	\$0	Scheme 3	\$0	Scheme 4	\$0
STRUCTURAL AND ARCHITECTURAL COSTS							
Scheme 1	\$35,000	Scheme 2	\$70,000	Scheme 3	\$45,000	Scheme 4	\$45,000
ENHANCED HURRICANE PROTECTION AREA (EHPA)							
Scheme 1	\$0	Scheme 2	\$0	Scheme 3	\$0	Scheme 4	\$0
CHEMICA		IT COST					
Scheme 1	\$29,000	Scheme 2	\$33,000	Scheme 3	\$20,000	Scheme 4	\$20,000
TEST AND BALANCE SERVICES							
Scheme 1	\$880	Scheme 2	\$1,720	Scheme 3	\$1,920	Scheme 4	\$1,760
DEMOLITION, DISPOSAL, GENERAL CONDITIONS							
Scheme 1	\$100,000	Scheme 2	\$100,000	Scheme 3	\$100,000	Scheme 4	\$100,000
TOTAL, ESTIMATED GROSS OR INITIAL COST TO INSTALL HVAC SYSTEM (with associated costs from above)							
Scheme 1	\$2,021,280	Seheme 2	\$2,477,920	Schome 2	\$2,460,320	Cabama 4	\$2,448,360

Engineer: Carastro & Associates, Inc.

Date: March 4, 2014

The costs listed on this page represent the engineer's opinion of probable cost. A licensed contractor should be consulted for accurate construction costs. <u>REFER TO PAGE 6 FOR A LIST OF ASSUMPTIONS MADE</u>.

#### LIFE CYCLE COST ANALYSIS

#### CHILLER PLANT UPGRADES - POLK STATE COLLEGE C&A # 5747

#### Data Sheet 5

Electricity cost estimates							
Scheme	Description	Chillers+ Towers	Pumps	Demand Charge Reduction	Chiller Plant Tota		
1	(2) Water Cooled Chillers, (2) Cooling Towers, variable primary flow	\$220,194	\$63,260	\$0	\$283,454		
2	(1) Water Cooled Chiller, (1) Cooling Tower, (2) Air Cooled Chillers, (18) Ice Tanks, (1) Heat Exchanger	\$337,193	\$69,028	\$31,140	\$375,081		
3	(3) Air Cooled Chillers, (30) loe Tanks, (1) Heat Exchanger	\$430,564	\$58,424	\$52,184	\$436,804		
4	(3) Air Cooled Chillers, (22) ice Tanks, (1) Heat Exchanger	\$371,496	\$53,700	\$43,937	\$381,259		
	Supp	plies and Labor esti	mates				
					\$5,00		
1	Supplies						
	Labor \$10,000						
-	Supplies				\$5,500		
2	Labor			\$10,500			
3	Supplies						
-	Labor \$6,0						
	Supplies						
4	Labor				\$2,000		

The costs listed on this page represent the engineer's opinion of probable cost. A licensed contractor should be consulted for accurate construction costs. <u>REFER TO PAGE 6</u> FOR A LIST OF ASSUMPTIONS MADE.

#### LIFE CYCLE COST ANALYSIS

#### CHILLER PLANT UPGRADES - POLK STATE COLLEGE C&A # 5747

#### Data Sheet 6

The following assumptions were made while assembling this brief analysis:

- Annual electricity costs used in this calculation are only those for chillers, cooling towers and pumps.
- Equipment sizing shown on this form is based on preliminary evaluations and shall be reviewed and revised during a chiller plant design project.

Engineer: Carastro & Associates, Inc.

Date: March 4, 2014

The costs listed on this page represent the engineer's opinion of probable cost. A licensed contractor should be consulted for accurate construction costs. REFER TO PAGE & FOR A LIST OF ASSUMPTIONS MADE.

# **APPENDIX B**

As an alternative to chemically treating the condenser water, we recommend reviewing the system designed by Water Conservation Technology International. It consists of one or multiple water softeners and controls monitored on a regular basis that offer significant water savings. Below, you will find an example of potential savings on a 1,200 ton chiller plant. In this example, the net water savings exceed \$29,000 per year and the system's payback is only twelve months.

If Polk State College wants to further research this item, we would gladly put together a presentation by the local manufacturer's representative.

Water Conservation 7 EQUIPMENT SELECTION U.S. Patents 6929749; 6949193; 69980 Use restricted to licensed Water and cost calculations are ba	8 PERFORMANC 292; 7122148; 7517493; 7 WCTI distributors ar	Martecol com			
1200 Tons	City	State	Distributor ⇒ Natural Green Chemistry		
Tower Information	Current	WCTI	Equipment Design Selections		
Tower / Evap Cooler Name =>	Tower 1	Tower 1	Click & Select Tons or RDT => Tons		
Tons Design Capacity =>	1200	1200			
	30.0	30.0			
Tons Design Evaporation GPM	1000	1000			
Tons Peak Load => Tons Peak Evaporation GPM	25.0	25.0			
	500	500			
Tons Average <sup>*</sup> Evaporation GPM	12.5	12.5	Select HES & HEF Models, then enter # Units (Tons or RTD)		
	3.0		\$ Units => 1		
	5,000		# Units => 0		
	75				
	70				
Current COC =>	2.5	50	<= ZBD / COC; depends on tower drift eliminators, water losses		
Blowdown / Water Loss GPM	8.3	0.3	<- Zero Tower BD, water losses only from drift or small leaks.		
Make-Up GPM	20.8	12.8			
Make-Up GPD	30,000	18,367			
Tower Makeup Water Ch	nemistry	# Note Actions	Below for Correct HES / HEF Design and Operation		
MU Peak TH (as CaCO3) 🖘	250	0.5	<= High MU Peak TH, use reduced HES Service Run below		
MU Avg^ TH (as CaCO3) =>	200	0.2			
Peak TDS ≕>	450				
Avg TDS =>	350				
Peak Turbidity NTU* =>	0.7	e- lifelbuunter Tud	bidity is normally low, so input "0" for Avg and Peak		
Avg Turbidity NTU* =>	0.2	<ul> <li>If city water, full</li> </ul>	buily is normally low, so input of for Avg and Peak		
MU Water \$102, Mg/L =>	10.0				
	10.0				
	0.5				
mo trator othornio, mgrc		1.5			
Regenerations per Day	Average <sup>^</sup> TH				
Gallons per HES Service Run	Average <sup>*</sup> TH	11,904	<= Modity HES (GrnPG) to match this Gallons per Service Run		
Standard Webs the Date for			st Savings Calculations		
Blowdown Water Use Reduction	GPM		** Enter current MU cost below, if no lower cost option		
Make-up cost /1000 Gais =>	Current MU		\$ 3.00 <= Enter lower oost source water **		
Blowdown cost /1000 Gals =>	Sewer / WWT		** Examples: Recycled WW; RO reject; Storm; Well water		
Load Hours (vs Avg* Tons) =>	Hours/Day		<= Do not reduce hours if Avg*Tons load input to B14		
Load Days (vs Avg^ Tons) 🖘	Days/Year	365			
Make-up Water Reduction	Gallons/Day	11,633			
Blowdown Water Reduction	Gallons/Day	11,633			
Current Annual Water Use	Gallons	10,950,000			
WCTI Annual Water Use	Gallons	6,704,082			
Annual Discussion of the second	Gallons	4,245,918			
Annual Blowdown Saved	• Maar	\$ 12,738			
Annual Blowdown Saved Make-up Water Savings	\$/Year				
	\$/Year				
Make-up Water Savings Blowdown Water Savings		\$ 16,984	Lower cost source water used by tower evaporation		
Make-up Water Savings Biowdown Water Savings Lower Cost Water Savings	\$/Year \$/Year	\$ 16,984 \$ -	Lower cost source water used by tower evaporation		
Make-up Water Savings Biowdown Water Savings Lower Cost Water Savings Total Water Savings	\$/Year \$/Year \$/Year	\$ 16,984 \$ - \$ 29,721	Lower cost source water used by tower evaporation		
Make-up Water Savings Biowdown Water Savings Lower Cost Water Savings Total Water Savings Regeneration Water Cost	\$/Year \$/Year \$/Year \$/Year	\$ 16,984 \$ - \$ 29,721 \$ 478	Lower cost source water used by tower evaporation		
Make-up Water Savings Biowdown Water Savings Lower Cost Water Savings Total Water Savings Regeneration Water Cost Net Water Savings	\$/Year \$/Year \$/Year \$/Year \$/Year	\$ 16,984 \$ - \$ 29,721 \$ 478 \$ 29,244			
Make-up Water Savings Biowdown Water Savings Lower Cost Water Savings Total Water Savings Regeneration Water Cost Net Water Savings	\$/Year \$/Year \$/Year \$/Year \$/Year Regenerate Water	\$ 16,984 \$ - \$ 29,721 \$ 478 \$ 29,244	<= Lower cost source water used by tower evaporation se and Cost Calculations Use clean salt		

3/25/2014

Gallons Per Day	187		4.0		
Gallons Per Year	68215		4.0	<= WCTI Design	
Salt Use / Day	Lb / Day		52	<- Daily use rates will be higher during peak loads / hardness	
Salt Cost / Lb	\$/Lb	\$	0.13	You can lower salt cost with use of Bulk Salt / Brine Maker	
Annual Salt Cost Lbs / Yr =>	19148	\$	2,489	Example, Bulk Brine Maker = \$80,000. Bulk salt cost \$0.04 / Lb.	
NET ANNUAL BD WATER \$AVING\$ (less salt oost)			26,755	TDS Lbs /Yr from current BD => 31,963	
WCTI	Pre-treatment Equ	ipn	pment Cost and Water Savings ROI Analysis		
HES Systems; # units / cost =>	1x HESDA-RPA 32	\$	14,300		
HEF Systems; # units / cost =>	0x Not Required A	\$	-		
Installation Cost Estimate	enter 0 or num ->	\$	10,000		
Shipping Cost Estimate enter 0 or num		\$	1,000	Example	
Equipment Cost Additions enter 0 or num		\$	750	Wireless hardware and service	
Total Equipment Cost		\$	26,050		
Equipment ROI (water savings) Months (R			12		
WCTI Distributor Program Fee Annual Cost		\$	14,000	Example	
Prior Chemical / Program Annual Cost		\$	7,500	Example	
Prior Maint (scale, corr, clean) Annual Cost		\$	5,000	Example	
Prior Prog + BD + Maint (- WCTI) Annual Cost		\$	25,255	Example	
WCTI Net Program Savings ROI Months (ROI)			12	Example	

3/25/2014